Lecture 15: The Mathematics of Water

Lecturer: Luis Cruz (for Brigita Urbanc) Office: 12-909 (E-mail: brigita@drexel.edu)

Course website: www.physics.drexel.edu/~brigita/COURSES/BIOPHYS_2011-2012/

11/15/2011

Water is of key importance in the living world.

Continuous description versus motion of individual H_20 molecules

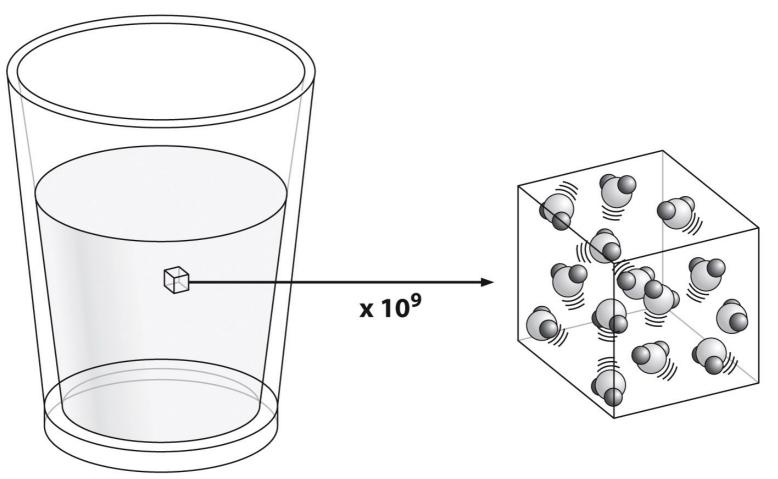
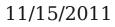


Figure 12.1 Physical Biology of the Cell (© Garland Science 2009)



Continuous description of water uses the velocity field, which in general can change with a spacial position (x,y,z) of a small volume of water and time:

 $\mathbf{v}(\mathbf{r},t)$

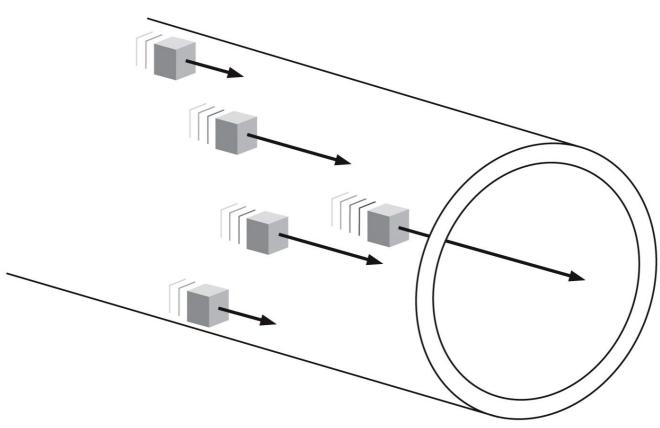


Figure 12.2 Physical Biology of the Cell (© Garland Science 2009)

Q: What distinguishes liquids from solids?

A: Solids and liquids respond to applied forces differently: Solids undergo deformation, liquids flow.

Mechanical properties of liquids are described by *viscosity* (in analogy to Young modulus E that describes solids).

For simple, Newtonian fluids: pulling force Results in a constant velocity fluid motion:

 $\frac{F}{A} = \eta \frac{V}{d}$

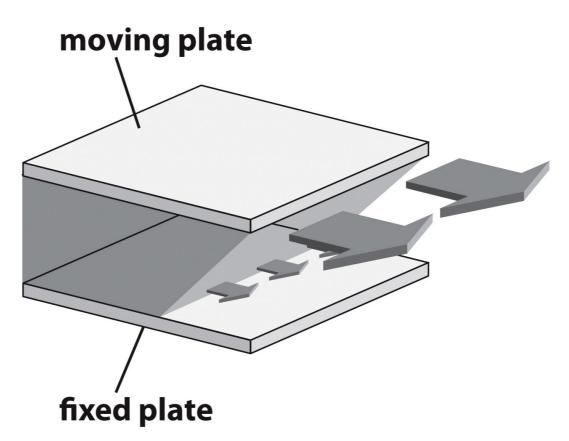


Figure 12.3 Physical Biology of the Cell (© Garland Science 2009)

Viscosity: η [Pa·s], where 1Pa=10⁻⁵N/m²=10⁻⁵atm

Viscosity of water: $\eta = 1 \text{ mPa} \cdot \text{s} = 10^{-8} \text{ N/m}^2 \cdot \text{s} = 10^{-8} \text{ atm} \cdot \text{s}$

Equation of motion for a Newtonian fluid: F=m**a**

Consider a small fluid element and apply Newton's second law to its motion:

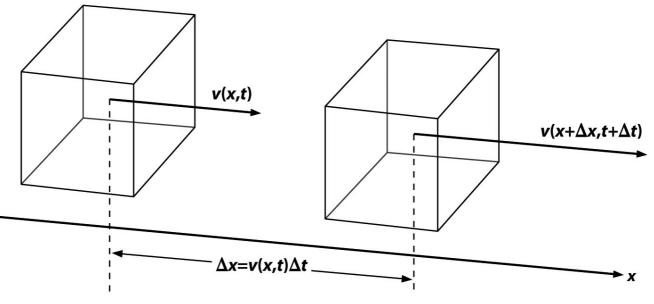
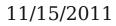


Figure 12.4 Physical Biology of the Cell (© Garland Science 2009)



In general, we need to consider: $\mathbf{r} = (\mathbf{x}, \mathbf{v}, \mathbf{z})$ $\mathbf{v} = (\mathbf{v}_x, \mathbf{v}_y, \mathbf{v}_z)$

To derive the equation of motion, we will assume a one-dimensional **Problem**:

$$\mathbf{v}(\mathbf{x}, \mathbf{t}) = \mathbf{v}(\mathbf{x}, \mathbf{t}) \mathbf{e}_{\mathbf{x}} \qquad \mathbf{e}_{\mathbf{x}} \dots \text{ unit vector along } \mathbf{x} - \text{direction}$$
$$\mathbf{v}(\mathbf{x} + \Delta \mathbf{x}, \mathbf{t} + \Delta \mathbf{t}) = \mathbf{v}(\mathbf{x}, \mathbf{t}) + \frac{\partial \mathbf{v}}{\partial \mathbf{x}} \Delta \mathbf{x} + \frac{\partial \mathbf{v}}{\partial \mathbf{t}} \Delta \mathbf{t}$$

The element moves along the x-direction by Δx in time Δt :

$$\mathbf{v}(\mathbf{x},\mathbf{t}) = \frac{\Delta \mathbf{x}}{\Delta \mathbf{t}} \quad \rightarrow \quad \frac{\partial \mathbf{v}}{\partial \mathbf{x}} \Delta \mathbf{x} = \frac{\partial \mathbf{v}}{\partial \mathbf{x}} \cdot \frac{\Delta \mathbf{x}}{\Delta \mathbf{t}} \cdot \Delta \mathbf{t} = \frac{\partial \mathbf{v}}{\partial \mathbf{x}} \cdot \mathbf{v} \cdot \Delta \mathbf{t}$$

Thus we can calculate the change of velocity and thus acceleration along the x-direction: $\begin{bmatrix} \partial y & \partial y \end{bmatrix}$

$$\Delta \mathbf{v}(\mathbf{x}, \mathbf{t}) = \left[\frac{\partial \mathbf{v}}{\partial \mathbf{t}} + \mathbf{v}(\mathbf{x}, \mathbf{t}) \frac{\partial \mathbf{v}}{\partial \mathbf{x}} \right] \Delta \mathbf{t} \rightarrow$$
$$\mathbf{a}(\mathbf{x}, \mathbf{t}) = \frac{\Delta \mathbf{v}(\mathbf{x}, \mathbf{t})}{\Delta \mathbf{t}} = \frac{\partial \mathbf{v}(\mathbf{x}, \mathbf{t})}{\partial \mathbf{t}} + \mathbf{v}(\mathbf{x}, \mathbf{t}) \frac{\partial \mathbf{v}(\mathbf{x}, \mathbf{t})}{\partial \mathbf{x}}$$

11/15/2011

We can express the acceleration of a fluid element at position **x** and at time t as a *material derivative*: $\mathbf{a} = \frac{\mathsf{D} \mathbf{v}}{\mathsf{D} + \mathsf{D}}$

which is defined as:
$$\frac{D}{Dt} = \frac{\partial}{\partial t} + \mathbf{v} \cdot \nabla$$

Material derivative consists of two parts:

- (1) conventional explicit time dependence reflecting the field variable v that is changing with time
- (2) convective term: a material particle can be dragged into a region of space, where the field is different
- Example of a temperature field T(x, t): (1) fluid is resting but T is changing with time (e.g. heating): $\frac{D}{Dt} = \frac{\partial}{\partial t}$

(2) fluid is moving, steady state T gradient:

$$\frac{\mathsf{D}}{\mathsf{Dt}} = \mathbf{v}_{\mathsf{x}} \cdot \nabla$$

Two different kinds of forces are acting on a fluid volume element

 $\Delta \mathbf{x} \times \Delta \mathbf{y} \times \Delta \mathbf{z}$

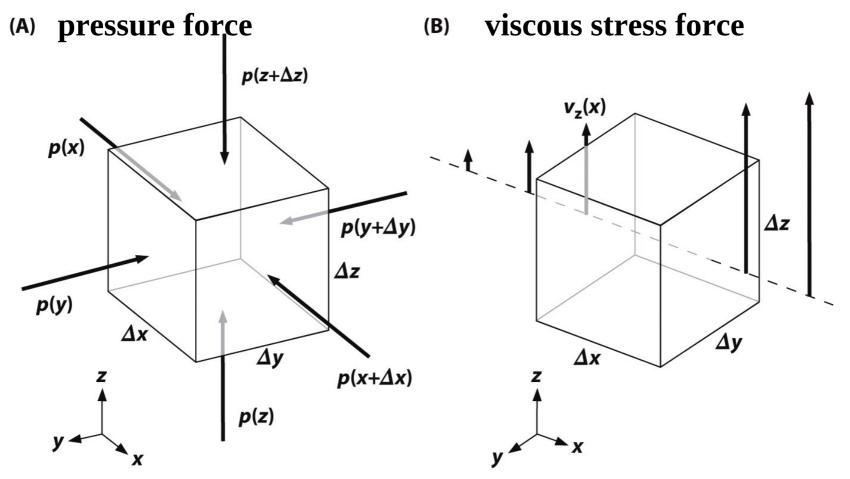


Figure 12.5 Physical Biology of the Cell (© Garland Science 2009)

Pressure Force: due to variations in the pressure along x, y, z Viscous Stress Force: friction on the volume element due to a velocity gradient along x, y, z

The total pressure force along the x-direction:

$$\delta \mathbf{F}_{x}^{p} = \mathbf{p}(\mathbf{x}, \mathbf{y}, \mathbf{z}, t) \Delta \mathbf{y} \Delta \mathbf{z} - \mathbf{p}(\mathbf{x} + \Delta \mathbf{x}, \mathbf{y}, \mathbf{z}, t) \Delta \mathbf{y} \Delta \mathbf{z}$$
$$\mathbf{p}(\mathbf{x} + \Delta \mathbf{x}, \mathbf{y}, \mathbf{z}, t) \approx \mathbf{p}(\mathbf{x}, \mathbf{y}, \mathbf{z}, t) + \frac{\partial \mathbf{p}}{\partial \mathbf{x}} \Delta \mathbf{x} \rightarrow$$
$$\delta \mathbf{F}^{p} = -\nabla \mathbf{p} \Delta \mathbf{x} \Delta \mathbf{y} \Delta \mathbf{z} \quad \text{where} \quad \nabla \mathbf{p} = \left(\frac{\partial \mathbf{p}}{\partial \mathbf{x}}, \frac{\partial \mathbf{p}}{\partial \mathbf{y}}, \frac{\partial \mathbf{p}}{\partial \mathbf{z}}\right)$$

The viscous force on the face at position x is: $-\eta \frac{\partial v_z(x)}{\partial x} \Delta y \Delta z e_z$ whereas on the face at position x + Δx is: $\partial v_z(x + \Delta x)$

$$+\eta \frac{\partial \mathbf{v}_{z}(\mathbf{x} + \Delta \mathbf{x})}{\partial \mathbf{x}} \Delta \mathbf{y} \Delta \mathbf{z} \mathbf{e}_{z}$$

11/15/2011

The total viscous stress force is then a sum of the two:

$$\delta F_{z}^{v} = -\eta \frac{\partial v_{z}(x)}{\partial x} \Delta y \Delta z \mathbf{e}_{z} + \eta \frac{\partial v_{z}(x + \Delta x)}{\partial x} \Delta y \Delta z \mathbf{e}_{z}$$
$$\frac{\partial v_{z}(x + \Delta x)}{\partial x} \approx \frac{\partial v_{z}(x)}{\partial x} + \frac{\partial^{2} v_{z}(x)}{\partial x^{2}} \Delta x$$
$$\delta F_{z}^{v} = \eta \frac{\partial^{2} v_{z}(x)}{\partial x^{2}} \Delta x \Delta y \Delta z$$

In general, the total viscous stress force can be written as:

$$\delta \mathbf{F}^{\mathbf{v}} = (\eta \nabla^2 \mathbf{v} + \eta \, \mathbf{\nabla} (\nabla \cdot \mathbf{v})) \Delta \mathbf{x} \Delta \mathbf{y} \Delta \mathbf{z}$$

If we only consider incompressible fluids, then $\nabla \cdot \mathbf{v} = 0$ and:

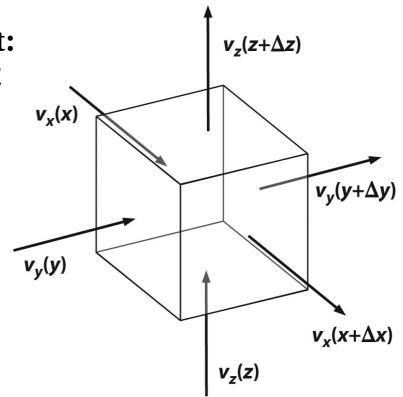
$$\delta \mathbf{F}^{\mathbf{v}} = \eta \nabla^2 \mathbf{v} \, \Delta \, \mathbf{x} \, \Delta \, \mathbf{y} \, \Delta \, \mathbf{z}$$

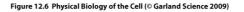
11/15/2011

Incompressible fluids: the flow can distort and stretch the fluid element but preserves its volume. Consider a volume element at a time t: $\Delta x \times \Delta y \times \Delta z$

A moment later, at $t + \Delta t$:

$$\Delta \mathbf{x'} = \Delta \mathbf{x} \left(1 + \frac{\partial \mathbf{v}_{\mathbf{x}}}{\partial \mathbf{x}} \Delta \mathbf{t} \right)$$
$$\Delta \mathbf{y'} = \Delta \mathbf{y} \left(1 + \frac{\partial \mathbf{v}_{\mathbf{y}}}{\partial \mathbf{y}} \Delta \mathbf{t} \right)$$
$$\Delta \mathbf{z'} = \Delta \mathbf{z} \left(1 + \frac{\partial \mathbf{v}_{\mathbf{z}}}{\partial \mathbf{z}} \Delta \mathbf{t} \right)$$





Thus the volume change is: $\Delta \mathbf{x}' \,\Delta \mathbf{y}' \,\Delta \mathbf{z}' = \Delta \mathbf{x} \,\Delta \mathbf{y} \,\Delta \mathbf{z} \left[1 + \left(\frac{\partial \mathbf{v}_{\mathbf{x}}}{\partial \mathbf{x}} + \frac{\partial \mathbf{v}_{\mathbf{y}}}{\partial \mathbf{y}} + \frac{\partial \mathbf{v}_{\mathbf{z}}}{\partial \mathbf{z}} \right) \right]$ $\Delta \mathbf{x}' \,\Delta \mathbf{y}' \,\Delta \mathbf{z}' = \Delta \mathbf{x} \,\Delta \mathbf{y} \,\Delta \mathbf{z} \left(1 + \nabla \cdot \mathbf{v} \right)$

11/15/2011

The Newtonian Fluid and the Navier-Stokes Equation

$$\Delta \mathbf{m} \mathbf{a} = \delta \mathbf{F}_{p} + \delta \mathbf{F}_{v} \quad \text{where} \quad \Delta \mathbf{m} = \rho \Delta \mathbf{x} \Delta \mathbf{y} \Delta \mathbf{z}$$
$$\frac{\partial \mathbf{v}}{\partial t} + (\mathbf{v} \cdot \nabla) \mathbf{v} = -\frac{1}{\rho} \nabla \mathbf{p} + v \nabla^{2} \mathbf{v} \quad \text{where} \quad v = \frac{\eta}{\rho}$$
kinematic viscosity

The Navier-Stokes equation is a second-order partial differential equation: need to specify the boundary conditions:

no-slip condition = at a solid boundary the fluid is at rest with respect to the solid

Fluid Dynamics of Blood

→ a process of blood circulation

- → blood vessels ranging in size from $2 \mu m$ to 1 cm
- → use cylindrical symmetry to describe the blood flow

$$\mathbf{v} = \mathbf{v}(\mathbf{r})\mathbf{e}_{z}$$

> consider only steady state:

$$\frac{\partial \mathbf{v}}{\partial t} = 0$$

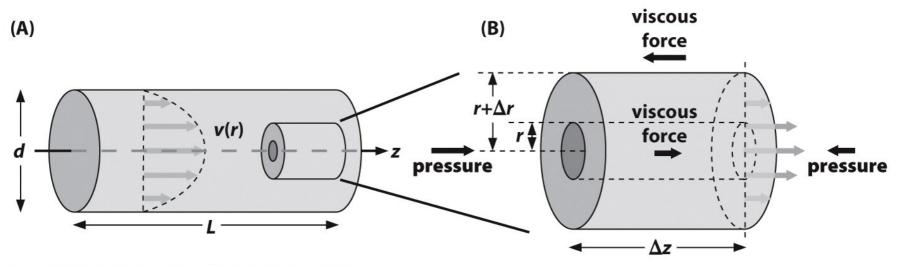


Figure 12.7 Physical Biology of the Cell (© Garland Science 2009)

Consider a small volume element in the shape of a hollow cylinder and calculate the opposing pressure forces:

$$\delta F_{z}^{p} = [p(z)-p(z+\Delta z)]2\pi r\Delta r = -\frac{dp}{dz}2\pi r\Delta r\Delta z$$

and the opposing viscous stress forces:

$$\delta F_{z}^{v} = \eta v'(r + \Delta r) 2 \pi (r + \Delta r) \Delta z - \eta v'(r) 2 \pi r \Delta z \text{ where } v' = \frac{dv}{dr}$$

Use the Taylor expansion:
$$v'(r + \Delta r) \approx v'(r) + \frac{dv'}{dr} \Delta r$$

To derive the expression for the viscous stress force:

$$\delta F_{z}^{v} = \eta v' 2\pi \Delta r \Delta z + \eta \frac{dv'}{dr} 2\pi r \Delta r \Delta z$$

In a steady state, a force balance on the hollow fluid cylinder is:

$$\delta \mathsf{F}_{z}^{\mathsf{p}} + \delta \mathsf{F}_{z}^{\mathsf{v}} = 0$$

11/15/2011

This results in a differential equation relating the pressure and velocity fields: $1 dp = 1 dy = d^2y = 1 d (dy)$

$$\frac{1}{\eta}\frac{dp}{dz} = \frac{1}{r}\frac{dv}{dr} + \frac{d^2v}{dr^2} \neq \frac{1}{r}\frac{d}{dr}\left(r\frac{dv}{dr}\right)$$

Laplacian of the velocity field in cylindrical coordinates

How do we solve this equation? Integrate both sides along the z direction along the length L:

$$\frac{-1}{\eta} \Delta p = \frac{1}{r} \frac{d}{dr} \left(r \frac{dv}{dr} \right) L \text{ where } \Delta p = p(0) - p(L)$$

pressure drop along the length of the pipe

Now integrate twice along r to get a solution:

$$\mathbf{v}(\mathbf{r}) = -\frac{\Delta \mathbf{p}}{\eta \mathbf{L}} \left(\frac{\mathbf{r}^2}{4} - \frac{\mathbf{C}_1}{\mathbf{r}^2} + \mathbf{C}_2 \right)$$

11/15/2011

Take into account the boundary conditions:

$$v(r=0) < \infty \rightarrow C_1 = 0$$

 $v\left(r=\frac{d}{2}\right) = 0$ no-slip $\rightarrow C_2 = \frac{-d^2}{16}$

We derive the final expression for the fluid velocity in the pipe:

$$\mathbf{v}(\mathbf{r}) = \frac{\Delta \mathbf{p}}{4 \eta L} \left(\frac{\mathbf{d}^2}{4} - \mathbf{r}^2 \right)$$

The fluid moves the fastest in the center of the pipe and not at all at the boundaries. We need an average velocity $\langle v \rangle$ which can be related to the flow rate Q: $Q = \frac{\langle v \rangle \pi d^2}{4}$

The average velocity and the resulting flow rate are:

$$\langle \mathbf{v} \rangle = \frac{\int_0^{d/2} \mathbf{v}(\mathbf{r}) 2\pi \mathbf{r} \, d\mathbf{r}}{\frac{\pi \, d^2}{4}} = \frac{\Delta \, \mathbf{p} \, d^4}{128 \, \eta \, \mathbf{L}} \quad \rightarrow \quad \mathbf{Q} = \frac{\pi \, \Delta \, \mathbf{p} \, d^4}{128 \, \eta \, \mathbf{L}}$$

11/15/2011

Estimated blood flow through capillaries: $d \approx 5 \mu m$ for most animals A measured pressure difference across a capillary and its length: $\Delta p \approx 20 \text{ mmHg} \approx 3000 \text{ Pa}$

 $L \approx 1 \text{ cm}$

The average flow velocity through a capillary:

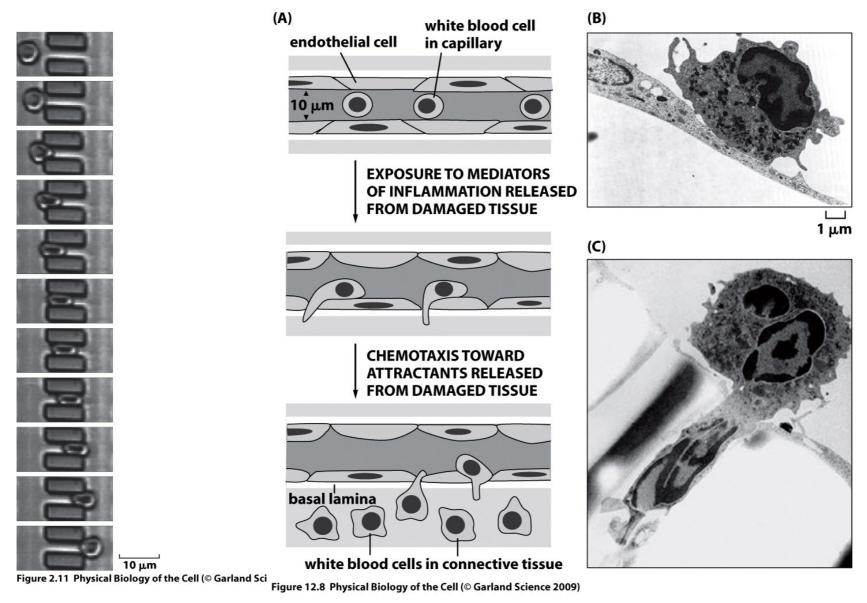
$$\mathbf{v} = \frac{\Delta p d^2}{32 \eta L} \approx 0.02 \,\mathrm{cm/s} \quad (\eta \approx \eta_{\mathrm{water}} = 10^{-3} \,\mathrm{Pa})$$

But the viscosity of blood is higher than that of water:

$$\begin{split} \eta &\approx 3\,\eta_{\,\text{water}} &\rightarrow v \approx 0.007 \,\,\text{cm/s} & \text{too small!} \\ v_{\text{measured}} &\approx 0.05 \,\,\text{cm/s} \end{split}$$

Can blood be well represented as a Newtonian liquid? Not really.

Blood carries red blood cells and white blood cells (leukocytes)



11/15/2011

The Low Reynolds number World

The 100 years experiment with a very viscous fluid: 1 drop every 10 years!

This system has the same viscous properties as water to the *E. coli* bacterium.

What is a Reynolds number Re? Re = intertial term of N.-S. Eq. / visocus term of N.-S. Eq.

For a rigid body of length L moving with a speed U:



Figure 12.9 Physical Biology of the Cell (© Garland Science 2009)

Re.N. = $\frac{\rho U^2/L}{n U/L^2} = \frac{\rho L U}{n} = \frac{L U}{v}$

For small Reynolds numbers, the Navier-Stokes equation simplifies into the Stokes equation:

$$abla \mathbf{p} = \eta \nabla^2 \mathbf{v}$$
 incompressibility: $\nabla \cdot \mathbf{v} = 0$

The meaning of Reynolds number can be found by comparing the kinetic energy to the work done by the viscous stress dissipation of an object of linear dimension a and speed u (where u/a is the rate of change of the fluid velocity):

$$\mathsf{KE} \approx \rho \, \mathsf{a}^3 \mathsf{u}^2 \qquad \mathsf{W} \approx \eta \frac{\mathsf{u}}{\mathsf{a}} \times \mathsf{a}^2 \times \mathsf{a} \quad \rightarrow \quad \mathsf{Re.N.} = \frac{\mathsf{KE}}{\mathsf{W}} = \frac{\mathsf{a}\,\mathsf{u}}{v}$$

Another way: compare the time needed to dissipate KE of the fluid element to the time needed to move a distance comparable to its size:

$$\tau_{\text{viscous}} = \frac{\rho a^2}{\eta} \ll \tau_{\text{inertial}} = \frac{a}{u} \rightarrow \text{Re.N.} = \frac{\tau_{\text{viscous}}}{\tau_{\text{inertial}}}$$

11/15/2011

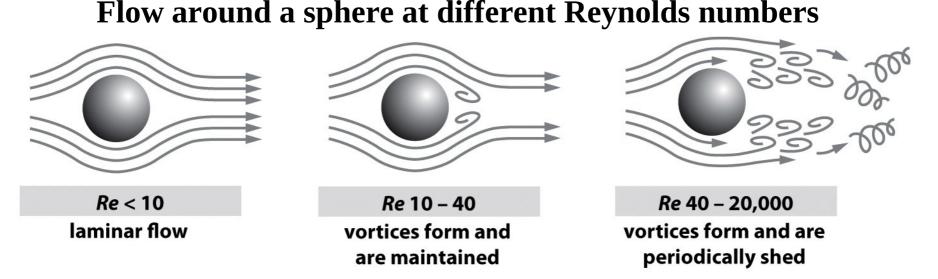


Figure 12.10 Physical Biology of the Cell (© Garland Science 2009)

The Stokes formula for a drag force on a sphere

- reed to integrate the viscous stress and the pressure over the surface of a sphere $\frac{V}{R}$
- → viscous stress proportional to the spatial derivative of the speed
- \rightarrow the area of the surface of the sphere: $4\pi R^2$
- → the Stokes force/drag is then: $F_s = C \eta \frac{V}{R} \times 4 \pi R^2 = 6 \pi \eta R v$

Stokes Drag in Single-Molecule Experiments

- → ATP synthase is a rotary motor
- actin filament attached to this motor is tagged by a fluorescent molecule
- → when the motor rotates, the filament spins around and the fluorescent tag allows us to measure the rotation
- * existence of pauses in molecular motors

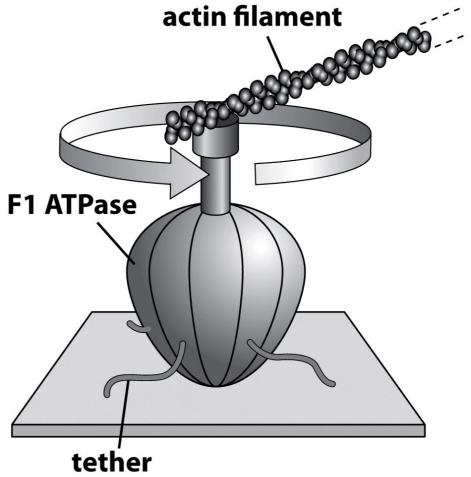
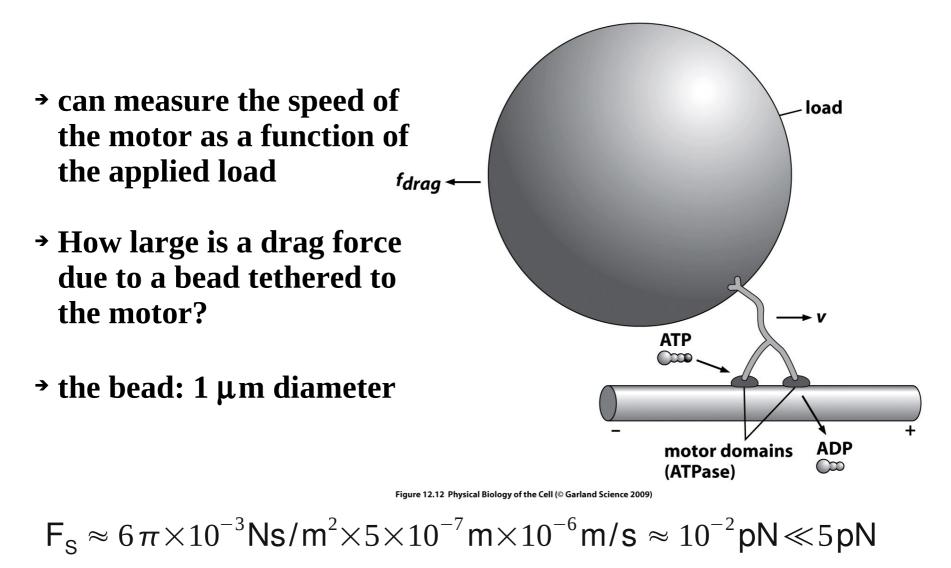


Figure 12.11 Physical Biology of the Cell (© Garland Science 2009)

Molecular motor: Motion of myosin on an actin filament position (nm) time (s) Figure 3.26b Physical Biology of the Cell (© Garland Science 2009) **Position as a function of time** ~5 nm

Figure 3.26a Physical Biology of the Cell (© Garland Science 2009)

Stokes Drag can be Neglected in Optical Tweezers Experiments



Dissipative Time Scales and the Reynolds Number

Consider a damped harmonic oscillator and analyze its behavior at low Reynolds numbers: $d^2x dx$

$$m\frac{d^2x}{dt^2} + \gamma\frac{dx}{dt} + kx = 0$$

 $\tau_{\rm viscous}$

A low Reynolds number means that the time scale over which the kinetic energy dissipates is small: $\frac{m(dx/dt)^2}{dt} \approx \gamma (dx/dt)^2$

(rate of dissipation on the right is a viscous force times velocity) Thus we get a simple expression: $\tau_{viscous} = \frac{m}{v}$

which means that we can neglect the inertial term in the equation and get $y \frac{dx}{dt} + kx = 0$ with a solution: $x(t) = x_0 e^{-(k/y)t}$

11/15/2011

Observation of stopping distances for objects of different sizes: Consider a spherical object with initial velocity equal to a diameter of a sphere per second

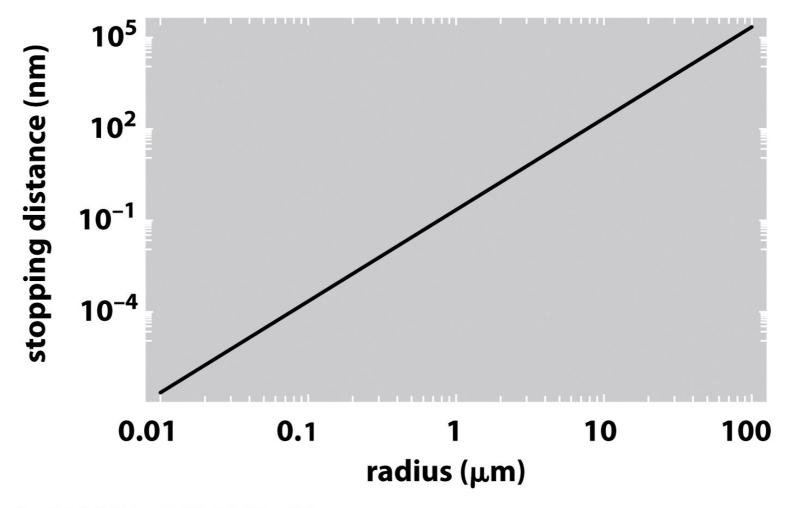


Figure 12.13 Physical Biology of the Cell (© Garland Science 2009)

E. coli moves by rotating its flagella

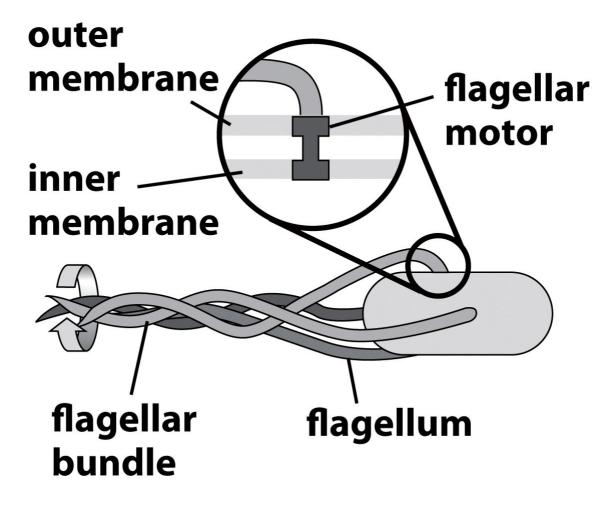
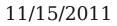


Figure 4.16a Physical Biology of the Cell (© Garland Science 2009)



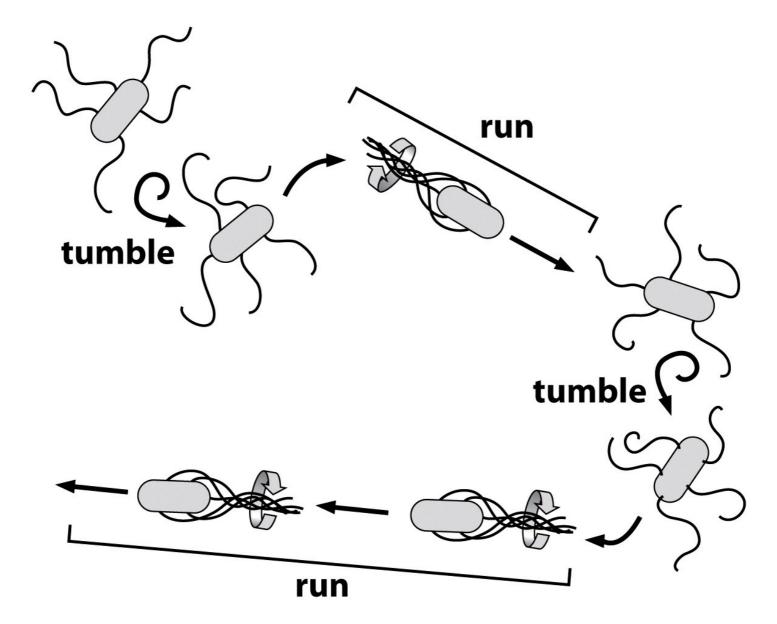


Figure 4.16b Physical Biology of the Cell (© Garland Science 2009)

Helically shaped flagella with a diameter D and pitch P:

 $D \approx 0.5 \,\mu$ m... diameter of the helically shaped flagellum $P \approx 2 \,\mu$ m... pitch of the helix (length of one helical turn) f... propulsion frequency $v = \pi D f...$ linear velocity

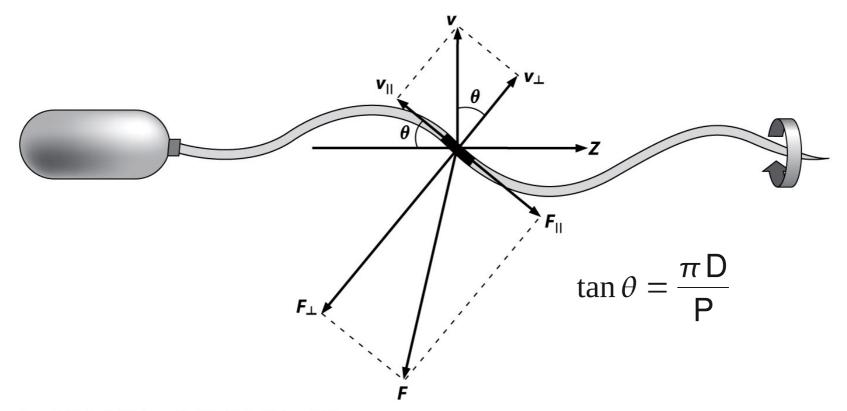


Figure 12.14 Physical Biology of the Cell (© Garland Science 2009)

The propulsive force relies on the difference in the drag coefficients between parallel and perpendicular motion of a rod:

→ force parallel to the rod is:

 $F_{\parallel} = \gamma_{\parallel} v \sin \theta$, where $\gamma_{\parallel} = 2 \pi v L$

→ force perpendicular to the rod is:

 $F_{\perp} = \gamma_{\perp} v \sin \theta$, where $\gamma_{\perp} = 4 \pi v L$

→ the total force projected onto the negative z-direction (direction of motion) is then: $F_{D} = -F_{\parallel}\cos\theta + F_{\perp}\sin\theta$

 $F_{p} = -2\pi\eta L v \sin\theta \cos\theta + 4\pi\eta L v \cos\theta \sin\theta = 2\pi\eta L v \sin\theta \cos\theta$

→ the propulsion force is balanced by the drag force:

$$\mathsf{F}_{\mathsf{D}} = 2\,\pi\,\eta\,\mathsf{L}\,\mathsf{V}$$

> which results in the final speed of:

 $V = \pi Df \sin \theta \cos \theta \approx 70 \,\mu \text{m/s} \quad (30 \,\mu \text{m/s exp.}) \quad (v = \pi Df)$ 11/15/2011 PHYS 461 & 561, Fall 2011-2012

Centrifugation and Sedimentation

- → biochemical purification: to separate macromolecules or their complexes from the solution
- *centrifugation*: a simple example of diffusion in the presence of drift using the Stokes formula
- → What is centrifugation? Spinning at up to 100,000 rpm ~ 10⁶ g
- → the centrifugal force that all molecules in the solution experience: $m\omega^2 r$
- → assume: the size of the sample much smaller than the distance from the rotation axis
- → The mass of the molecule in the solvent needs to be corrected by the mass of displaced solvent: $m \rightarrow (\rho_P \rho)V$

The centrifugal force imparts a drift velocity to the biomolecules (low Reynolds numbers): centrifugal force equal to the frictional Force: $v_{drift} = \frac{mg_c}{\gamma}$ for a sphereical molecule: $\gamma = 6\pi\eta R$

The quantity m/γ is quoted for different biomolecules in units of Svedberg: 1 svedberg = 10^{-13} s

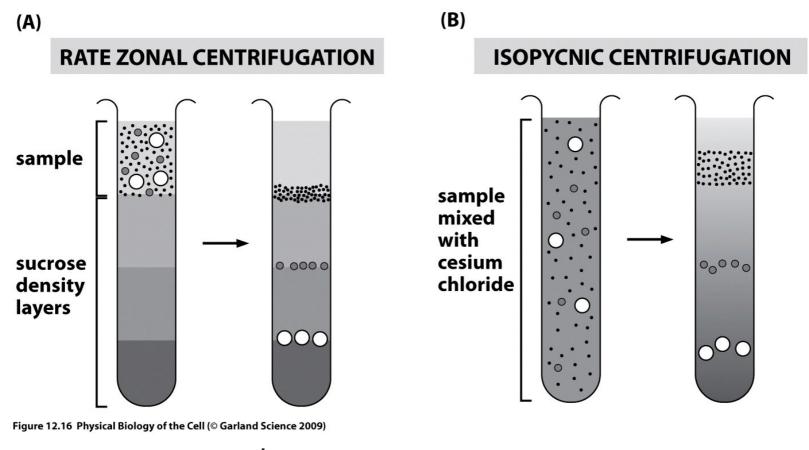
which corresponds to a globular protein with a radius of 1 nm in water. Typical density of proteins: 1.35g/cm³

The drift velocity is then a quadratic function of the size of the Biomolecule: $(\rho_{-}-\rho)4/3\pi B^{3} - 2(\rho_{-}-\rho)$

$$\mathbf{v}_{\text{drift}} = \frac{(\rho_{\text{P}} - \rho) 4/3\pi R}{6\pi\eta R} = \frac{2(\rho_{\text{P}} - \rho)}{9\eta} R^2 g_{\text{c}}$$

which allows for an effective separation of particles based on their respective sizes.

Rate Zonal Versus Isopycnic Centrifugation



$$\mathbf{x}_{c} = \mathbf{v}_{drift} \mathbf{t}$$

 $\Delta \mathbf{x} = \sqrt{2 \, \mathrm{D} \, \mathrm{t}}$

Diffusion of biomolecules due to thermal fluctuations: a negative effect on the separation. A condition for separation:

$$|v_{drift1} - v_{drift2}|t > (\sqrt{2D_1} + \sqrt{2D_2})\sqrt{t}$$

which shows that we just need to wait long enough for two types of molecules to separate:

$$\mathbf{t}_{\mathsf{sep}} = \left(\frac{\sqrt{2} \mathbf{D}_1 + \sqrt{2} \mathbf{D}_2}{\left| \mathbf{v}_{\mathsf{drift1}} - \mathbf{v}_{\mathsf{drift2}} \right|} \right)$$

However, a test tube has a finite length, so the separation needs to occur before the molecules reach the bottom of the tube, that is, the speed of spinning needs to be large enough:

$$v_{\text{drift}} t_{\text{sep}} < L \quad \rightarrow \quad g_{\text{c}} > \frac{1}{L} \frac{m_1}{\gamma_1} \left(\frac{\sqrt{2D_1} + \sqrt{2D_2}}{m_1/\gamma_1 - m_2/\gamma_2} \right)^2$$

The other separation method: isopycnic centrifugation relies on a density gradient of the solvent and different densities of the various macromolecules that needs to be separated.